

**Final Report**

US EPA RECORDS CENTER REGION 5



1007446

# **Treatability Study: Air Sparging/Soil Vapor Extraction System**

**Amphenol Franklin Power Products  
Franklin, Indiana**

**May 1999**



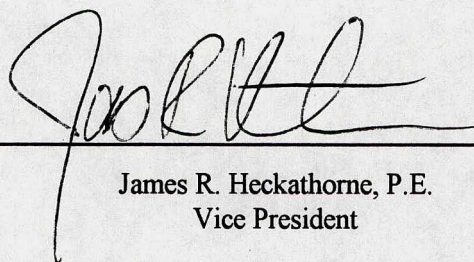
**O'BRIEN & GERE**  
ENGINEERS, INC.



REPORT

**Treatability Study:  
Air Sparging/Soil Vapor Extraction System**

*Amphenol Franklin Power Products  
Franklin, Indiana*



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## 1. Introduction

This report presents the results of the air sparging/soil vapor extraction (AS/SVE) pilot study conducted at Amphenol/Franklin Power Products facility in Franklin, Indiana. The pilot study was conducted in compliance with Section VIII. F and Attachment A, Task III of the Administrative Order on Consent U.S. EPA I.D. # IND 044 587 848. This report also presents basis of design considerations for a full scale AS/SVE system, based on the pilot study results.

### 1.1. Site background

The Amphenol/Franklin Power Products facility covers an area of approximately 15 acres. The property is bounded on the east by Hurricane Road, on the south by Hamilton Street, on the north by an abandoned rail line, and on the west and northwest by a Farm Bureau Co-Op facility and Arvin Industries, respectively. To the south, southeast, and southwest, the land use is primarily residential. A site location map is included as Figure 1.

The main structure on the site is a 46,000 square foot building formerly used in the manufacture and distribution of electrical components. This building was built in 1961 by Dage Electric, Inc. for the manufacture of electric connectors. The operation was acquired in 1963 by Bendix Corporation for its Bendix Connector Operations plant. Processes included electroplating, machining, assembling and storing manufactured components. From 1961 to 1981, wastewater from plating operations at the facility was discharged directly into a municipal sanitary sewer. In 1981, a wastewater pretreatment system was installed in a separate building for treatment of cyanide and chromium bearing wastewater from the plating room. New wastewater lines were installed from the plating room to the pretreatment building, with the effluent from the pretreatment plant routed to a sanitary sewer manhole just south of the main manufacturing building. In 1983, the Bendix Corporation was acquired by Allied Corporation and merged with its Amphenol Products Division. As a result of consolidation efforts, manufacturing at the Franklin facility ceased in September 1983 and the plant was closed at that time.



Closure of RCRA units began in February 1984. In 1986, Amphenol Products Division became the Amphenol Corporation, and in 1987 it was sold and became a wholly owned subsidiary of LPL Investment Group, Inc. Amphenol sold the facility to Franklin Power Products, Inc. on June 15, 1989.

A hydrogeologic investigation of the facility was initiated in February 1984 by Allied Corporation concurrent with plant closure activities, and in anticipation of the sale of the property. The investigation entailed the collection and analysis of soil samples and groundwater samples for volatile and semi-volatile organic compounds, pesticides/PCBs, EP TOX metals and cyanide. A total of 10 volatile organic compounds (VOCs) were detected in ground water. In particular, elevated concentrations of tetrachloroethene (PCE) and trichloroethene (TCE) were detected in wells adjacent to the main facility building, particularly along the southwest corner adjacent to the plating room. The sanitary sewer line and the soils beneath the plating room were also investigated.

A second hydrogeologic investigation began in February 1985 to develop a more comprehensive characterization of ground water flow, ground water quality and contaminant transport on and near the property. The investigation included the collection of ground water samples from existing monitoring wells, sampling of the storm sewer discharge, and sampling of the Hurricane Creek surface water. A variety of VOCs were detected in ground water samples, storm sewer discharge samples, and Hurricane Creek surface water samples. The greatest level of contaminants appeared to be concentrated in areas south of the former plating room. Six additional monitoring wells were installed and sampled. Analytical results obtained from the ground water samples indicated that the storm drain along the south boundary was acting as a partial ground water intercept. Additionally, 27 soil borings were installed along the west and south sides of the former plating room. Minimal contaminant concentrations were detected in the samples obtained from the soil borings. In each sample, total VOC content was less than 3 ppm.

In September of 1985, a ground water monitoring plan was submitted to the Indiana State Board of Health and implemented in February 1986. Results obtained during the ground water monitoring program were generally similar to the results obtained during the 1985 hydrogeologic investigation.

The following closure and corrective measures activities were conducted at the Amphenol facility in response to the previously described investigations:



- Removed and disposed of plating room floor and soil beneath the floor to a depth of nine feet. The excavation was treated with sodium hydroxide. Clean backfill and a new concrete floor were provided;
- Disconnected and plugged the old sanitary sewer line and replaced it with a new line offset 35 feet east of the old one;
- Drained and treated fluids from the wastewater treatment system, the plating room tanks and other areas in the plating room;
- Drained and treated liquid from the underground cyanide overflow tank, and capped the pipes at the discharge end; and
- Removed twelve previously installed ground water monitoring wells and grouted the boreholes to the surface.

In 1990, an Administrative Order on Consent was signed by respondents Franklin Power Products and Amphenol Corporation. Respondents were responsible for conducting a Resource Conservation and Recovery Act Facility Investigation (RFI). RFI field activities began in January 1992 and work was performed in accordance with the approved RFI Work Plan. RFI investigations were performed from 1992 through 1994.

RFI investigations indicated that past practices at the former Amphenol site involved the disposal of chlorinated solvents to the sanitary sewer. Leaking joints in the vitrified clay sanitary sewer, and a failure of the sewer where it crosses over a 72-inch storm sewer line caused chlorinated solvents to be released into the environment. The primary area of concern is proximate to the sanitary sewer line failure. During periods of high ground water levels, the storm sewer intersects the ground water table allowing VOCs to enter.

Based on the results of the RFI and with concurrence of the USEPA, respondents initiated the design and implementation of an interim corrective measure (ICM) in August 1994. The purpose of the ICM was to remediate ground water using a pump-and-treat system, and to depress the surface water to a level below the storm sewer thereby limiting the release of VOC constituents to Hurricane Creek. The respondents are also responsible for conducting a Corrective Measures Study (CMS). The purpose of the CMS was to evaluate applicable and appropriate remedial technologies based on the findings of the RFI and site characteristics. The corrective measure presented in the CMS included institutional controls, on and off-site ground water monitoring for VOCs, and monitoring of VOCs in on-site soil. Data collected from the monitoring wells will allow more effective observation of the level and fate of VOCs in soil and ground water and will allow



monitoring of effects of continued operation of the existing extraction wells and air stripper (ICM). Additionally, the CMS recommended the implementation of a focused, on-site AS/SVE pilot test program to evaluate whether this technology was suitable for the site.

## **1.2. Purpose and objective**

The purpose of the AS/SVE pilot study was to evaluate the feasibility of this technology to supplement the existing ground water recovery system and enhance the removal of VOCs from ground water in the vicinity of the storm sewer. The objective of this pilot study was to identify an effective radius of influence and basis of design parameters that may be used to assist in the design of a full scale AS/SVE system.



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## 2. Air Sparging/Soil Vapor Extraction Pilot Study

The pilot study was completed to evaluate the application of AS and SVE at the subject site. The results of this effort were used to develop the conceptual preliminary design.

The pilot program consisted of installation of pilot study wells and field testing of AS and SVE systems. Below is a summary of the activities performed and the results obtained.

### 2.1. Pilot study equipment

To conduct the study, a temporary AS/SVE pilot system was installed on-site. The system consisted of two AS injection wells (ASI-1 and ASI-2), two monitoring locations (MON-1 and MON-2), and an SVE well (SVE-1). The location and configurations of the AS/SVE well system are shown on Figures 3 and 4, respectively.

ASI-1 and ASI-2 were installed to the bottom of the silty sand unit, located approximately 20 feet below ground surface (bgs). The injection wells were constructed of 2-inch ID PVC having 2 ft sections of 0.01-inch slot screens at the bottom. The monitoring locations are approximately 5 ft and 8 ft away from ASI-1. Each monitoring location consists of two 1 1/4-inch ID PVC monitoring points fitted with a 2 ft bottom well screen. One monitoring point was installed in the saturated zone to a depth of approximately 18 ft bgs, and one point was installed in the unsaturated zone to a depth of approximately 8 ft bgs. A 3 ft thick bentonite plug was installed between the lower and upper monitoring points in each borehole to minimize interference between the lower and upper monitoring points. In addition to the MON-1 and MON-2 monitoring points, existing monitoring well MW-22, located approximately 10 ft from ASI-1, was also utilized during the study. AS injection wells and monitoring well locations are presented on Figure 3.

The soil vapor extraction well, SVE-1, was installed to a depth of 8 ft, approximating the unsaturated portion of the silty sand unit (beneath the



glacial till unit). SVE-1 was constructed of 2-inch ID PVC with a 2 ft section of 0.01-inch slot screen at the bottom. Monitoring points MON-1 and MON-2, described above, also served as monitoring points for the SVE tests.

The AS equipment provided on the temporary, trailer mounted AS/SVE system included a carbon vane compressor with up stream/down stream pressure gauges, flow control valve and flow meter. The SVE equipment included a regenerative blower with an upstream liquid separator, and suction/discharge piping. The piping included a vacuum gauge, flow control valve, and flow meter.

Field monitoring equipment included pressure and temperature gages, a water level probe, dissolved oxygen (DO) meter, a photoionization detector (PID), helium detector, velocity meter (velometer), temperature gauge, and Draeger tubes.

## **2.2. Pilot study description**

After baseline testing, the pilot study was conducted in three phases as summarized on Table 1. The first phase was the AS test, the second phase was the SVE test, and the third phase was the combined AS/SVE test.

The Phase I AS test was conducted to evaluate the radius of influence of injected air into the shallow ground water at the site. Compressed air injected into the saturated subsurface forms air bubbles which travel horizontally and vertically away from the injection point. To monitor the distances the air bubbles travel from the point of injection, a helium tracer was added.

The AS pilot study was initially run at a flow rate of approximately 6 cfm, at a pressure of 3 pounds per square inch-gauge (psig), with a helium flow rate of 10 liters per minute. Due to minimal increase in DO concentrations at monitoring locations, the AS flow rate was increased to 8 CFM after 7 hours. The flow rate was then increased to approximately 10 CFM after an additional 21 hours and to 12 CFM after an additional 20 hours.

During the AS pilot study, dissolved oxygen, helium, and ground water levels were measured at monitoring points MON-1D, MON-2D and MW-22. In addition to the evaluation of the radius of influence, the response of VOC



concentrations to AS was also evaluated. VOC concentrations in ground water were monitored at MON-1 and MON-2, prior to, during, and after performance of the pilot study. Sampling frequency is summarized in Table 1. Sampling data is included in Appendix A.

The Phase II SVE test was conducted to evaluate the radius of influence of the extraction wells in the vadose zone at the site.

The SVE test was initially performed at 50 CFM at approximately 20 inches of water column vacuum (in. H<sub>2</sub>O). Based on the low vapor concentrations and vadose zone pressure, the flow rate was increased to 100 CFM at 53 in. H<sub>2</sub>O after approximately 1 hour. The flow rate was momentarily increased to 120 CFM at 64 in. H<sub>2</sub>O after approximately 13 hours. Sediment was recovered from the SVE well at 120 CFM so the flow rate was reduced to 100 CFM for the duration of the test. The vacuum at the SVE well stabilized at approximately 48 in. H<sub>2</sub>O.

The application of a negative pressure to the vadose zone resulted in extraction of VOCs present in pore spaces disrupting the equilibrium between VOCs on the soil and in the soil vapor. Air extracted during SVE test was sampled for VOCs using TCE and PCE specific Draeger tubes temporarily installed in the discharge stack of the SVE system. In addition, pressures in monitoring points (MON-1S and MON-2S) were measured to evaluate responses to varying extraction rates and partial vacuum on SVE-1. Sampling frequencies are summarized in Table 1. Sampling data is included in Appendix A.

In addition to operating both AS and SVE systems separately, a Phase III - combined AS/SVE test was conducted. The purpose of the combined test was to evaluate the effectiveness of SVE capture of AS generated soil gas. During this phase of the pilot study, air was injected into the saturated zone via ASI-1 and ASI-2, while air was extracted from the unsaturated vadose zone via SVE-1. The combined phase of the pilot study lasted for seven days. During this phase of the pilot study, ASI-1 was operated at 6 CFM and 10 CFM, ASI-2 was operated at 6 CFM, and SVE-1 was operated at 75 CFM. Sampling frequencies are summarized in Table 1. Sampling data is included in Appendix A.



### 2.3. Pilot study results

*Phase I - AS test.* The radius of influence from AS was evaluated by monitoring increases in the concentration of DO in groundwater in monitoring wells/points. A DO concentration increase above background generally indicates that the ground water point is within the area of influence of the AS well. An increase in the vadose zone VOC concentrations in monitoring wells provides an indication that organic compounds are being stripped from the ground water and transferred to the vadose zone. An increase in vadose zone pressure in monitoring wells provides an indication of the zone of influence of sparged air after it leaves the saturated zone.

DO concentrations taken before the start of the AS test indicated background concentrations of approximately 1 to 5 milligrams per liter (mg/L). The DO concentrations in MON-2D and MW-22 were extremely variable throughout the test. A slight but a general increase was observed in MON-1D. Based on this information, the AS radius of influence was determined to be approximately 5 ft. The radius of influence from an AS well is commonly in the range of 1 to 1.5 times the depth of the top of the sparge point below the ground water surface. Since the baseline water level in the injection well was approximately 4 ft above the top of the screened section, the radius of influence found at this site is within the expected range of approximately 4 to 6 ft.

Helium concentrations taken before the start of the air sparging test indicated no background trace of helium. Helium concentrations increased and decreased, consistent with changes in the amount of helium injected into the air stream, for MON-1S, MON-2S, and MW-22. The other monitoring wells did not indicate significant changes over background concentrations during the AS test.

Increases in the VOC concentrations at all of the monitoring locations with screened sections in the vadose zone indicate that organic compounds were being stripped from the groundwater and transferred to the vadose zone. Increases in the pressure in those monitoring wells indicated that sparge air migration was occurring in the vadose zone.

*Phase II - SVE test.* The vacuum measurements recorded at MON-1S and MON-2S were used to evaluate the radius of influence from the SVE pilot study. A vacuum less than - 0.01 inches of water (in. of H<sub>2</sub>O) has been used at other sites to define the effective radius of influence, or the distance at which sufficient air flow is believed to exist for remediation of the vadose zone. Vacuums were observed at MON-2S and MW-22 of approximately



-0.80 and -0.08 in.  $H_2O$ , respectively. Vacuum was not observed at MON-1S, which is approximately 8 feet from SVE-1. The reason for a lack of vacuum at MON-1S is unknown. However, it is conjectured that the effective radius of influence may be somewhat linear along the 72-inch storm sewer. The radius of influence along the sewer line is unknown since only one well was installed along the sewer backfill. The effective radius of influence appeared to extend into the natural formation for a distance of 15 to 20 ft.

The effective radius of influence was observed to be less than expected at the SVE flow rate. This may be due to the proximity of the SVE well to the sewer line.

*Phase III - AS/SVE test.* During the AS/SVE phase of the pilot study, pressures were recorded at MON-1S and MW-22 of approximately 0.01 and 0.23 in.  $H_2O$ , respectively. Positive pressure indicates that the extraction well is not causing a vacuum in the vadose zone and therefore is not effectively capturing the sparged air.

*Vapor sample results.* The concentrations of TCE and PCE in the exhaust from the SVE blower were monitored periodically with Draeger tubes throughout the SVE and AS/SVE phase of the pilot study. The concentrations of TCE in the blower exhaust were below detection limits throughout the test. The concentrations of PCE in the blower exhaust varied from below detection limits to approximately 10 parts per million (ppm), with an average of approximately 2 ppm. A PID was also used to quantitatively monitor VOCs from the blower exhaust and the monitoring locations. The concentration of VOCs in the blower exhaust varied from approximately 0.7 to 18 ppm, with an average resultant of approximately 2 ppm. The concentrations of VOCs at the monitoring wells varied from non-detectable concentrations to approximately 73 ppm at MW-22 with the PID. Using PCE Draeger tube measurement data and the formula provided in Appendix B, the average removal rate of PCE during the pilot study was approximately 0.005 pounds per hour.

## 2.4. Feasibility evaluation

The design of a full scale AS/SVE system is contingent on results obtained during the pilot study. To evaluate the feasibility of this technology for the subject site, it will be assumed that individual injection points will exhibit a 5 ft radius of influence and extraction points will exhibit an approximately 20 ft radius of influence.



Based on the assumed radius of influences, a full scale AS/SVE system would consist of 80 injection wells and 9 extraction wells distributed across an area of approximately 200 ft by 40 ft. The approximate size and location of the treatment area is presented on Figure 2. A total of 89 wells would need to be installed in order to achieve overlapping cones of influence across the treatment area. Due to the large number of wells required to effectively cover the treatment area, this technology may not be feasible for this site.

## **2.5. Conclusions**

As stated above, the results of the pilot study indicated that SVE removed PCE from the vadose zone at a rate of approximately 0.005 pounds per hour. With new well upgrades to the on-site ground water recovery system, installed as part the ICM described above, PCE detected in influent is approximately 1600 parts per billion and the average pumping rate of the four recovery wells is approximately 26 gallons per minute. Analytical results of the effluent data show that treated water discharged from the ground water recovery system is clean. The ground water recovery system effectively removes PCE from the ground water at a rate of approximately 0.02 pounds per hour. Due to the large number of wells required for the AS/SVE system and the relatively low expected PCE recovery rate, the design and installation of a full scale system is not recommended. Further evaluation and possible enhancement of the upgraded on-site ground water recovery system is recommended as a feasible remedial alternative to the AS/SVE system.



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## References

Gabriel, William J, CPG (O'Brien & Gere). Letter to Samuel Waldo (Amphenol/Franklin Power Products) Re: AS/SVE pilot study plan. February 25, 1999.

Hanford, C. Todd (Burns & McDonnell Waste Consultants, Inc.). Letter to Judy Rank (O'Brien & Gere) Re: Summary of pilot testing activities. April 15, 1999.



Table 1. Sampling and monitoring activities

Phase	Media	Sample frequency	Location	Parameter (Method/instrument)
Baseline testing (prior to initiation of each of the 3 pilot tests)	ground water	Twice a day for one day	ASI-1, ASI-2, MON-1D, MON-2D, MW-22	static water level (probe) DO (DO meter) VOCs (PID)
	ground water	One time before sparge test	MON-1D, MON-2D	VOCS (USEPA 8021)
	soil gas	Twice a day for one day	MON-1S, MON-2S, SVE well	VOCs (PID) helium (helium meter)
During all test operations	air	Continuous*	breathing zone (4 to 7 ft above ground in vicinity of monitoring points and SVE system)	VOCs (PID)
Phase 1: air sparging test	ground water	1 hr into test, 3 hrs into test, 6 hrs into test; every 6 hours thereafter*	MON-1D, MON-2D, MW- 22	DO (DO meter) helium (air within wells) static water level (probe)
Test duration: 3 days	ground water	during air sparge test	MON-1D MON-2D	VOCS (USEPA 8021)
	soil gas	1 hr into test, 3 hrs into test, 6 hrs into test; every 6 hours thereafter*	MON-1S, MON-2S	helium (helium meter) VOCs (PID) vapor pressure
	air flow to AS well	1 hr into test, 3 hrs into test, 6 hrs into test; every 6 hours thereafter*	ASI-1	air flow helium flow
	air flow		Blower/ compressor discharge	air pressure
Phase 2: soil vapor extraction test	soil gas	30 min into test, 1 hr into test, 3 hrs into test, 6 hrs into test; every 6 hours thereafter*	MON-1S, MON-2S	vapor pressure
Test duration: 3 days	ground water	30 min into test, 1 hr into test, 3 hrs into test, 6 hrs into test; every 6 hours thereafter*	ASI-1, ASI-2, MON-1D, MON-2D, MW-22	static water level (probe)
	extracted vapors	30 min into test, 1 hr into test, 3 hrs into test, 6 hrs into test; every 6 hours thereafter*	SVE-1	VOCs (Dräger tubes) air flow rate

May 4, 1999

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O'Brien & Gere Engineers, Inc.



**Table 1. Sampling and monitoring activities**

Phase	Media	Sample frequency	Location	Parameter (Method/instrument)
Phase 3: combined air sparging and soil vapor extraction test  Test duration: 7 days	ground water	30 min into test, 1 hr into test, 3 hrs into test, 6 hrs into test; every 4 hours thereafter*	MON-1D, MON-2D, MW-22	DO (DO meter) static water level (probe)
	soil gas	30 min into test, 1 hr into test, 3 hrs into test, 6 hrs into test; every 4 hours thereafter*	MON-1S, MON-2S	VOCs (PID) vapor pressure
	air to AS well	30 min into test, 1 hr into test, 3 hrs into test, 6 hrs into test; every 4 hours thereafter*	ASI-1, ASI-2	air flow rate
	extracted vapors	30 min into test, 1 hr into test, 3 hrs into test, 6 hrs into test; every 4 hours thereafter*	SVE-1	VOCs (Dräger tubes)
Following pilot test	ground water	Once	MON-1D, MON-2D	VOCs (USEPA 8021) DO (DO meter) static water level (probe) helium (helium meter, air within wells)
	soil gas	Once	MON-1S, MON-2S	VOCs (PID) helium (helium meter)

**Notes:**

\* Tests envisioned to be attended 10 - 12 hours daily, with monitoring only performed during attended hours.

MON-1S and MON-2S denote the monitoring points screened in the unsaturated zone.

MON-1D and MON-2D denote the monitoring points screened in saturated zone.

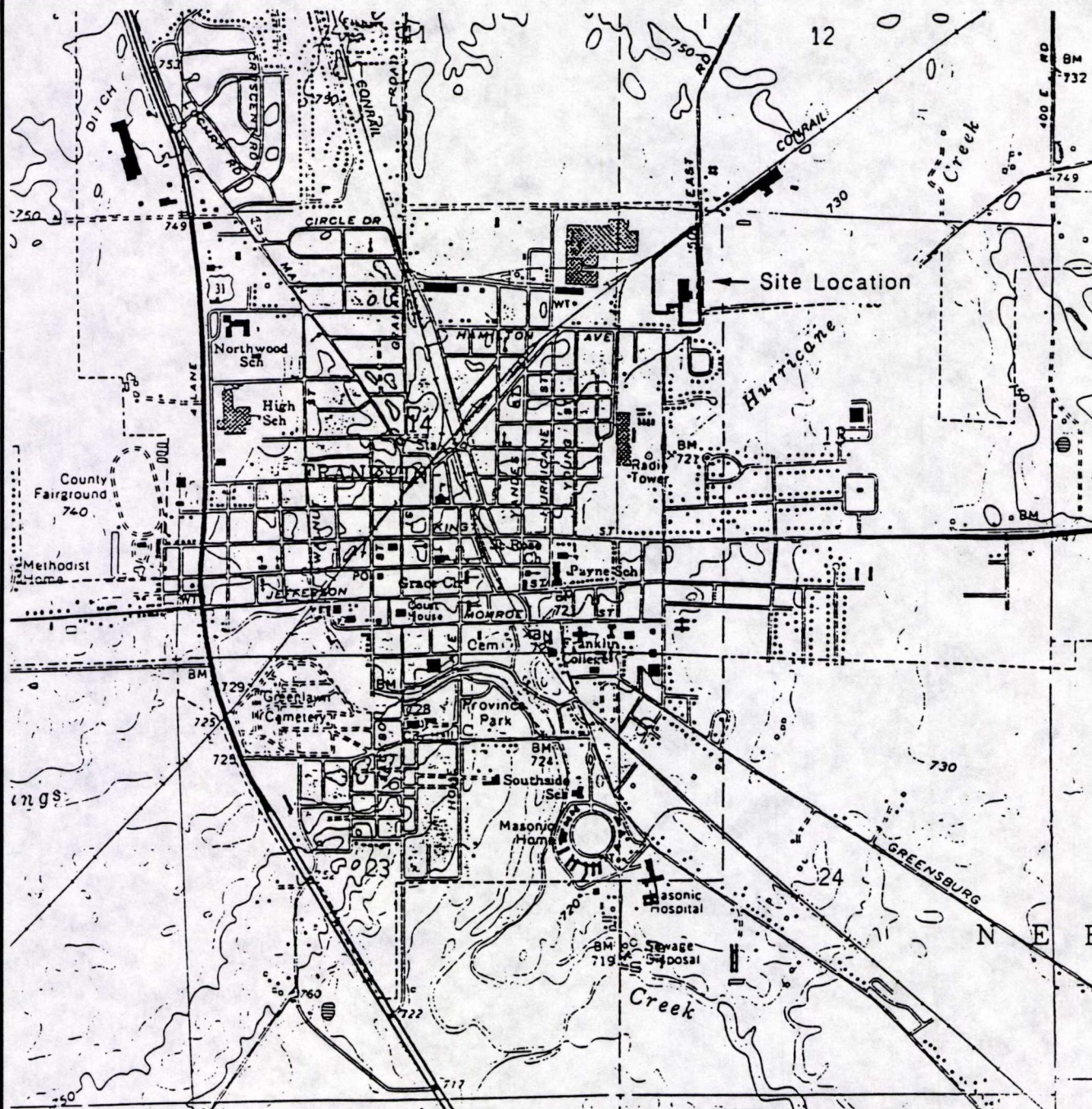
Dräger tubes for TCE and PCE.

May 4, 1999

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O'Brien & Gere Engineers, Inc.

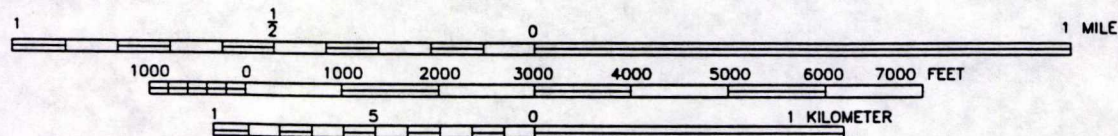




SOURCE: ADAPTED FROM U.S.G.S. FRANKLIN, INDIANA 7.5' TOPOGRAPHIC QUAD.



# AMPHENOL CORP. FRANKLIN POWER PRODUCTS FACILITY SITE LOCATION MAP



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FIGURE 2

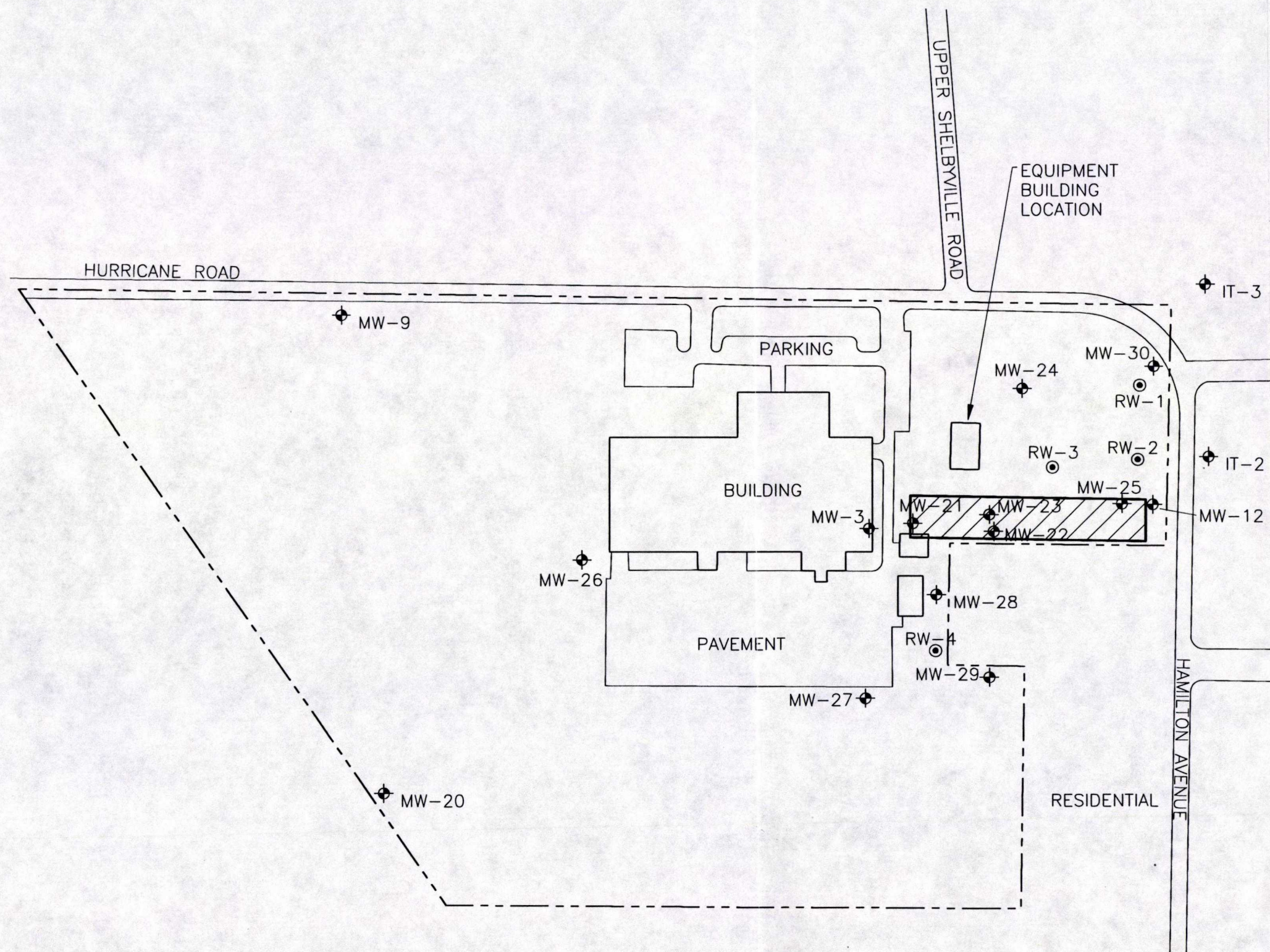


**LEGEND**

PROPERTY LINE

MONITORING WELL LOCATION

RECOVERY WELL LOCATION



**AMPHENOL CORP.  
FRANKLIN POWER PRODUCTS  
FACILITY**

**SITE MAP**



MARCH 1999  
FILE NO.3729.21493- 004



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FIGURE 3



LEGEND

- ⊕ APPROXIMATE MONITORING WELL LOCATION
- APPROXIMATE ASI LOCATION
- APPROXIMATE SVE LOCATION

AMPHENOL CORP.  
FRANKLIN POWER PRODUCTS  
FACILITY

AIR SPARGING/  
SOIL VAPOR EXTRACTION  
WELL LOCATIONS



APRIL 1999  
3729.21493-001



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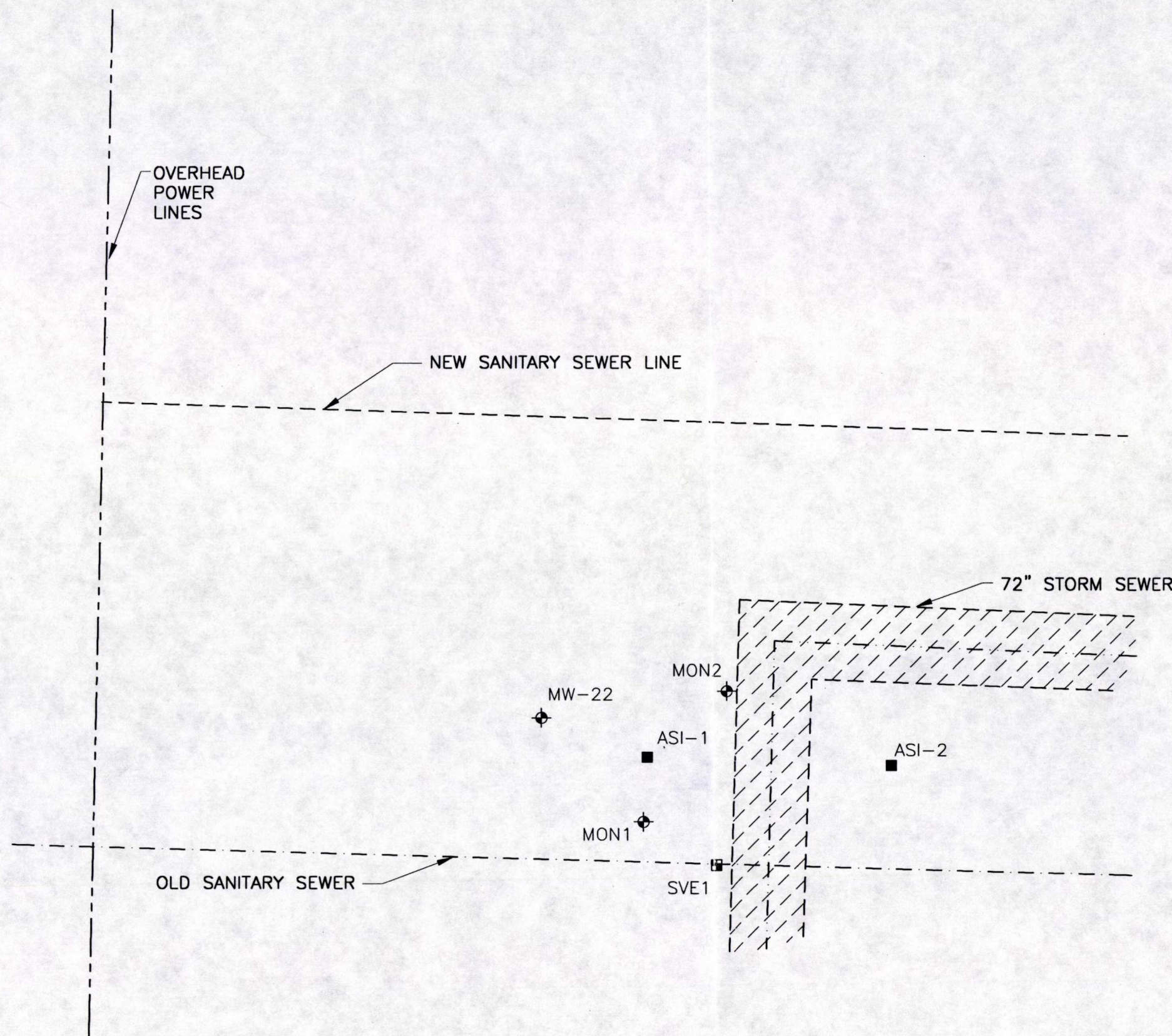
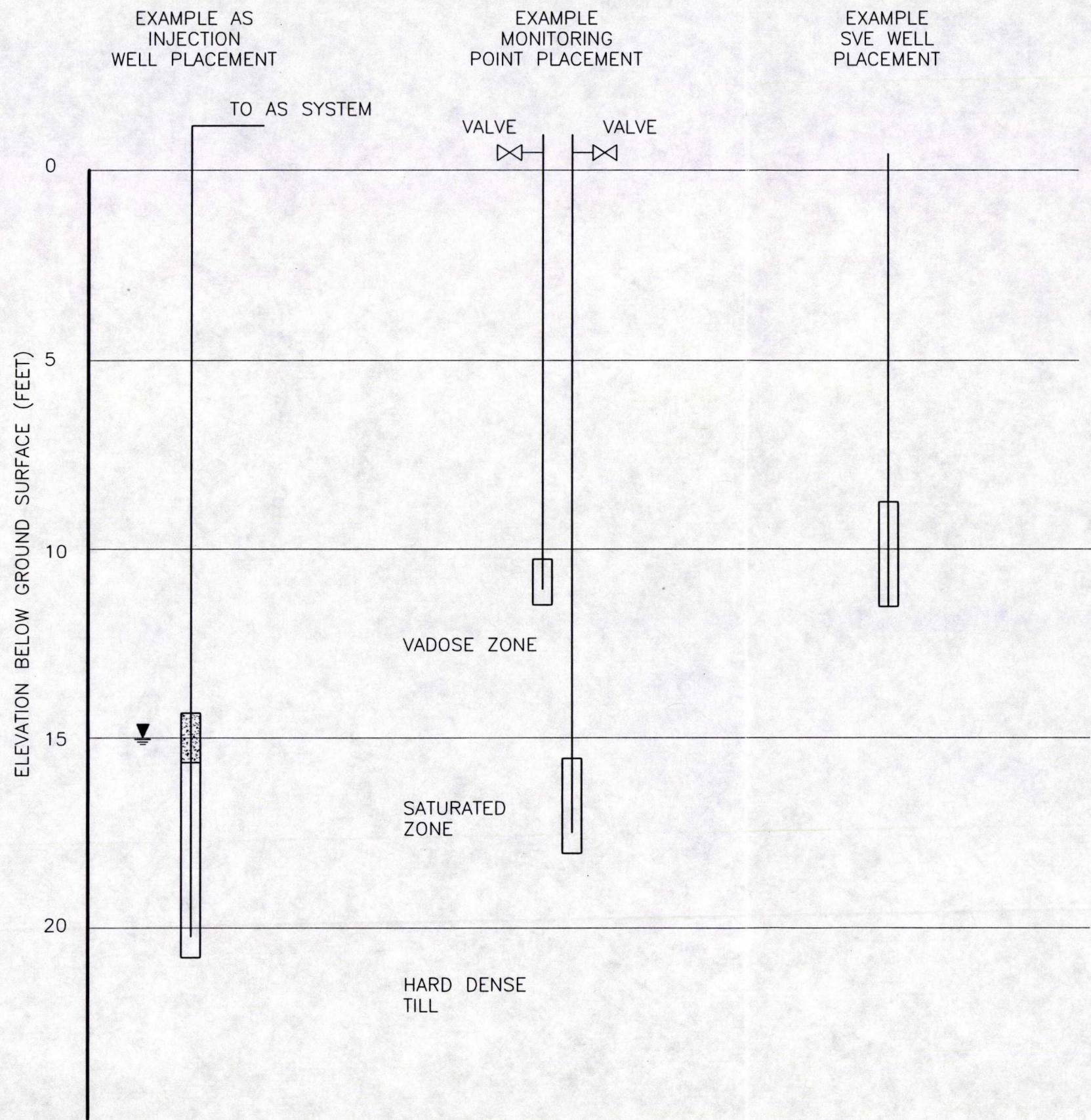




FIGURE 4



AMPHENOL CORP.  
FRANKLIN POWER PRODUCTS  
FACILITY

PILOT STUDY  
WELL  
SCHEMATIC

NOT TO SCALE

APRIL 1999  
3729.21493-002





**Sampling and monitoring data**



# Air Sparging Pilot Study Data

Date	3/23/99					3/24/99			3/25/99			3/26/99
Time	9:00	12:30	13:40	15:50	18:40	7:40	13:40	18:40	7:30	11:45	17:40	7:30
Flow (CFM)												
ASI-1	6	6	6	6	8	8	8	12	12	10	10	12
Helium Flow (% of air flow)												
ASI-1	0	4.9	1.8	3.2	0.65	0	0.59	--	0	1.1	--	--
Pressure (psi)												
ASI-1	0	3	3	3	2.5	2	2	2.6	1.25	1.25	--	2
Depth to GW (ft)												
MON-1D	15.94	15.77	15.89	15.94	15.94	15.94	15.94	15.56	15.95	15.95	15.95	15.96
MON-2D	16.22	16.03	16.2	16.26	16.24	16.25	16.26	15.96	16.24	16.22	16.14	16.15
MW-22	16.82	16.51	16.74	16.8	16.79	16.81	16.8	16.56	16.8	16.79	16.75	16.8
Dissolved Oxygen (mg/L)												
MON-1D	5.03	5.82	5.08	6.33	5.92	5.92	6.46	--	--	--	6.84	6.04
MON-2D	3.67	7.75	6.78	2.43	2.42	5.3	3.68	--	--	--	7.04	6.09
MW-22	1.92	4.69	4.42	4.01	2.51	1.65	1.13	--	--	--	2.04	2.2
VOCs (PID - ppm)												
MON-1S	1.5	4	3.5	4.4	11	10.7	3.4	1.9	7.3	4.4	5.7	5.6
MON-1D	1.2	0.9	0.2	0	4.2	1.5	0	0	1.6	0	0	1.7
MON-2S	6	31	13.7	17.3	31.5	34	26.2	31.4	23.2	13.2	25.1	35.6
MON-2D	0.6	0	0.3	0	3.1	4.7	0	6.6	66.7	25.9	2.6	3.4
MW-22	18.5	11.1	73.4	63.5	58.8	46.2	26.6	57.7	32.7	33.6	32.3	24.3
Helium (ppm)												
MON-1S	0	0	5.6	0.28	0	0	0	0	0	0	0	0
MON-1D	0	0	0.01	0	0	0	0	0	0	0	0	0
MON-2S	0	0	1	3	0.8	0	0.05	0	0	0.09	0.9	0
MON-2D	0	0	0	0	0	0	0	0	0	0	0	0
MW-22	0	0	7.1	0.63	0.61	0.03	1.1	0	0.44	0.52	0.35	1.5

Notes: Baseline data was collected on March 23, 1999 at 0900.  
Phase I - AS test commenced on March 23, 1999 at approximately 1135.



# Soil Vapor Extraction Pilot Study

Date	3/26/99					3/27/99			3/28/99		
Time	14:35	17:00	17:40	18:15	19:30	7:15	13:00	18:20	7:40	12:40	18:10
Depth to GW (ft)											
MON-1D	15.96	15.96	15.96	15.96	15.96	15.97	15.96	15.97	15.98	15.98	15.98
MON-2D	16.25	16.26	16.25	16.26	16.26	16.25	16.26	16.26	16.26	16.26	16.27
MW-22	16.83	16.83	16.83	16.83	16.84	16.84	16.85	16.85	16.85	16.85	16.86
ASI-1	16.92	16.91	16.91	16.91	16.91	16.91	16.91	16.91	16.91	16.92	16.92
ASI-2	16.79	16.8	16.8	16.79	16.8	16.8	16.8	16.8	16.8	16.81	16.81
Vapor Pressure (in. H <sub>2</sub> O)											
MON-1S	0	0	0	0	0	0	0	0	0	0	0
MON-2S	0	0	0	-0.79	-0.79	-0.8	-2	-0.84	-0.8	-0.81	-0.76
Extracted Vapors											
(VOCs Draeger)											
SVE - 1 (ppm)											
TCE	--	--	0	0	0	0	0	0	0	0	0
PCE	--	--	0	10	5	2	5	2	2	2	1
Air Flow (CFM)	--	50	100	100	100	100	120	100	100	100	--

**Notes:** Baseline data was collected on March 26, 1999 at 1435.  
Phase II - SVE test commenced on March 26, 1999 at approximately 1630.



**Combined Air Sparging and Soil Vapor Extraction Pilot Study**

Date	3/29/99						3/30/99				
Time	8:15	9:40	10:15	12:20	13:50	18:00	6:00	12:00	15:30	16:30	17:30
<b>Water level (ft)</b>											
MON-1D	15.99	16.06	15.97	15.98	16.01	15.99	16.01	16.02	16	16.02	16.03
MON-2D	16.28	16.37	16.27	16.25	16.29	16.27	16.31	16.3	16.28	16.3	16.32
MW-22	16.87	16.99	16.84	16.82	16.87	16.87	16.89	16.89	16.85	16.87	16.89
<b>Dissolved Oxygen (mg/L)</b>											
MON-1D	7.47	7.41	8.86	8.35	8	8.18	8.73	8.7	8.22	8.39	8.28
MON-2D	7.56	8.58	0.82	0.69	1.15	8.53	7.51	7.13	6.52	7.43	7.47
MW-22	0.97	3.32	2.92	1.55	1.8	1.85	1.86	1.77	1.64	1.91	2.39
<b>Vapor Pressure (in. H<sub>2</sub>O)</b>											
MON-1S	0	0.01	0.015	0.015	0.015	0.01	0.01	0.005	0.01	0.01	0.01
MON-2S	< 0	< 0	< 0	< 0	< 0	0	< 0	< 0	< 0	< 0	< 0
<b>VOCs (PID - ppm)</b>											
MON-1S	1.1	0	0	0	0	0	0	0	0	0	0
MON-2S	0	0	0	0	0	0	0	0	0	0	0
<b>Air Flow Rates (CFM)</b>											
ASI-1	6	6	6	6	6	6	6	6	10	10	10
ASI-2	6	6	6	6	6	6	6	6	6	6	6
<b>Extracted Vapor</b>											
<b>SVE-1 (ppm)</b>											
TCE		0	0	0	0	0	0	0	0	0	0
PCE		2	1	2	1	1	1	2	1	1	1



**Combined Air Sparging and Soil Vapor Extraction Pilot Study**

Date	3/31/99				4/1/99				4/2/99			
Time	6:00	10:00	14:00	18:00	6:00	10:00	14:00	18:00	6:00	10:00	14:00	18:00
<b>Water level (ft)</b>												
MON-1D	16.03	16.03	16.04	16.04	16.03	16.03	16.03	16.03	16.06	16.06	16.04	16.05
MON-2D	16.31	16.3	16.31	16.31	16.31	16.31	16.31	16.33	16.33	16.33	16.34	16.33
MW-22	16.88	16.89	16.9	16.9	16.9	16.9	16.91	16.92	16.91	16.91	16.93	16.93
<b>Dissolved Oxygen (mg/L)</b>												
MON-1D	8.27	8.33	8.3	8.09	8.17	8.21	8.28	8.26	8.11	8.27	8.48	8.24
MON-2D	7.47	8.18	6.92	7.3	7.56	7.22	7.4	7.32	7.66	7.88	7.88	7.74
MW-22	2.28	1.66	2.15	1.87	1.91	2.02	1.29	1.86	1.47	1.31	1.57	1.46
<b>Vapor Pressure (in. H2O)</b>												
MON-1S	0.01	0.005	0.01	0.01	0.01	0.01	0.01	0.01	0.005	0.005	0.005	0.005
MON-2S	<0	<0	<0	<0	<0	<0	<0	<0	<0	<0	<0	<0
<b>VOCs (PID - ppm)</b>												
MON-1S	0	0	2	3.9	3.2	2.7	--	--	--	1	0.2	1.2
MON-2S	0	0	0	0	0	0	0	--	--	0	0	0
<b>Air Flow Rates (CFM)</b>												
ASI-1	10	10	10	10	10	10	10	10	10	10	10	10
ASI-2	6	6	6	6	6	6	6	6	6	6	6	6
<b>Extracted Vapor</b>												
<b>SVE-1 (ppm)</b>												
TCE	0	0	0	0	0	0	0	0	0	0	0	0
PCE	1	2	1	2	2	2	1	2	1	1	1	1



**Combined Air Sparging and Soil Vapor Extraction Pilot Study**

Date	4/3/99				4/4/99				4/5/99
Time	6:00	10:00	14:00	18:00	6:00	10:00	14:00	18:00	6:00
Water level (ft)									
MON-1D	16.06	16.06	16.04	16.05	16.06	16.06	16.05	16.04	16.05
MON-2D	16.33	16.33	16.35	16.33	16.33	16.33	16.36	16.35	16.35
MW-22	16.93	16.93	16.95	16.92	16.93	16.93	16.95	16.95	16.95
Dissolved Oxygen (mg/L)									
MON-1D	8.08	8.37	8.3	7.63	8.31	7.54	8.26	8.18	8.31
MON-2D	7.41	7.71	7.58	7.34	6.93	6.63	7.76	7.51	7.61
MW-22	1.57	1.62	1.46	1.47	1.31	1.42	1.47	1.4	1.42
Vapor Pressure (in. H2O)									
MON-1S	0.006	0.005	0.005	0.005	0.005	0.005	0.005	0.005	0.005
MON-2S	<0	<0	<0	<0	<0	<0	<0	<0	<0
VOCs (PID - ppm)									
MON-1S	1.2	1.6	0.8	1.4	1.2	1.2	0.6	0.6	0.6
MON-2S	0	0	0	0	0	0	0	0	0
Air Flow Rates (CFM)									
ASI-1	10	10	10	10	10	10	10	10	10
ASI-2	6	6	6	6	6	6	6	6	6
Extracted Vapor									
SVE-1 (ppm)									
TCE	0	0	0	0	0	--	--	--	--
PCE	1	1	1	2	2	--	--	--	--

**Notes:**

Baseline data was collected on March 29, 1999 at approximately 0815.  
Phase III - combined AS/SVE test commenced on March 29, 1999 at approximately 0900.



**Formulas and limits**



## Formulas and limits

### 1. Calculation of lbs/hour emissions from SVE stack

$$\frac{\text{lbs}}{\text{hr}} \text{ compound} = (x) (y) \frac{(8.2235 \times 10^{-5})}{(T + 460)} MW$$

$x$  = acfm air ( velocity (ft/min) x area of discharge pipe (ft<sup>2</sup>) )  
 $y$  = ppmv compound  
 $T$  = discharge temperature °F  
 $MW$  = molecular weight of compound

MW PCE: 165.85  
MW TCE: 131.40  
MW TCA: 133.42  
MW DCA: 98.96  
MW DCE: 96.94

### 2. Total VOC discharge maximum

5 lb/day maximum for TOTAL VOCs = 0.21 lbs/hr

**To account for Dräger tube inaccuracy, SVE system should operate at maximum calculated total VOC emissions of 0.105 lb/hr.**

### 3. Helium usage to be sufficient to be detectable with helium detection meter. Recommend at least 3% by volume. Only use helium during daily monitoring periods for air sparge test phase.



12 MAY 1988

Review of Quality Assurance Project Plan  
RFI Work Plan - Amphenol Corporation

William E. Muno, Acting Associate Director  
Office of RCRA

ORIGINAL SIGNED BY  
WILLIAM E. MUNO

James Adams, Chief  
Quality Assurance Office

Please review the enclosed Quality Assurance Project Plan and  
provide your comments to William Buller, RCRA Enforcement Branch,  
5HS-12.

We would appreciate a reply by June 9, 1988.

Enclosure

5HS-1:WBuller:nd:6-4568:5/9/88

*CMR 4/1/8*

	TYPIS	AUTHOR	OTHER STAFF	UNIT CHIEF	SECT. SECT.	SECT. CHIEF	ENTER CHIEF	WMD BRI
INIT. DATE	5/9/88 HLC	5/9/88 WB		JMB 5/9/88	AP 5/10/88	P. E. A 5-10-88	WEM 5/11	

*for J.B.*



1st  
Draft  
I Looked  
At.

DRAFT  
9/16/99

VIA FACSIMILE AND CERTIFIED MAIL  
RETURN RECEIPT REQUESTED

DE-9J

Mr. Samuel S. Waldo  
Director of Environmental Affairs  
Amphenol Corporation  
358 Hall Avenue  
P.O. Box 5030  
Wallingford, Connecticut

Re: Franklin Power Products, Inc./Amphenol  
Review of CMI Groundwater Recovery  
and Treatment System Upgrade Report,  
Treatability Study AS/SVE, and  
Webb Field Evaluation  
Franklin, Indiana  
IND 044 587 848

Dear Mr. Waldo:

The United States Environmental Protection Agency (U.S. EPA) has reviewed: the Corrective Measures Implementation (CMI) Groundwater Recovery and Treatment System Upgrade Report; the Treatability Study Air Sparging/Soil Vapor Extraction (AS/SVE) System Report; and the Webb Field Evaluation Report that were submitted to U.S. EPA on May 6, 1999, by O'Brien & Geere Engineers, Inc. on behalf of Franklin Power Products, Inc. and Amphenol Corporation.

Groundwater Recovery and Treatment System Upgrade Report

In general, U.S. EPA did not find the data presented in the Groundwater Recovery and Treatment System Upgrade Report to be of adequate quantity or quality to enable verification of the conclusions reached by the Report, specifically the conclusion regarding the containment of on-site groundwater. Specific comments are provided in the enclosure which specify the additional information that should be obtained and/or submitted to support the statements made in the Report.

The Groundwater Recovery and Treatment System Upgrade Report states that one of the objectives for replacing the recovery wells' pneumatic pumps with electric submersible pumps was to increase the groundwater withdrawal rates sufficiently to suppress the water level within the aquifer to an elevation below



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Section VII.E of the  
Consent order does Not  
specify a timeframe, but  
6 months seems  
reasonable

the invert elevation of a 72-inch diameter storm drain which crosses the site. Based on the data and statements (page 3) presented within the Report, this objective does not appear to have been accomplished. The Report recommends (page 3) a continuation of the groundwater elevation monitoring to determine whether continued pumping of the upgraded system will, over time, result in the dewatering of the water bearing zone, and lowering of the water table to an elevation below the storm sewer invert. U.S. EPA concurs with the recommendation for the short-term since the new pumps and additional extraction well have resulted in an overall increase in groundwater withdrawal rates. However, since the report indicates (page 3) that after approximately one month of pumping with the upgraded system the groundwater level adjacent to the storm sewer was still one foot above the invert of the storm sewer, U.S. EPA suggests that if the groundwater elevation adjacent to the storm sewer does not show a substantial continued decreasing trend during the first six months of operation, that Franklin be required to implement other measures to prevent continued groundwater infiltration to the storm sewer Pur Suant to Section VII.E. of the Consent order

#### Treatability Study: Air Sparging/Soil Vapor Extraction

Due to the nature of this document, U.S. EPA has not generated any deficiency comments, but rather provided the following information on the efficacy of the system. U.S. EPA reviewed the Amphenol Franklin Power Products Treatability Study: Air Sparging/Soil Vapor Extraction (AS/SVE) System Final Report (May 1999) prepared by O'Brien and Gere Engineers Inc. (Treatability Study). The primary objective of the Treatability Study was to evaluate the feasibility of using AS/SVE technology to supplement the existing groundwater recovery system and enhance the removal of VOCs from ground water in the vicinity of the storm sewer. The pilot study included the installation of two air sparge injection wells, one soil vapor extraction well and two new monitoring wells (equipped with both a shallow and deep monitoring point).

The treatability study consisted of three phases. In the first, only the air sparging portion of the system was operated and monitored. In the second phase, only the soil vapor extraction system was operated and monitored and in the third stage, both systems were operated in unison. Based on the information provided in the Treatability Study Report, it appears that the Treatability Study was performed and monitored in an appropriate manner. The Treatability Study results were used to determine an average perchloroethylene (PCE) removal rate for the study and to calculate a radius of influence for both the injection and extraction well points to establish an appropriate design for a



I am ok with this From a Technical Standpoint.  
 You may wish to specifically tell them whether  
 3 they have fulfilled the requirements  
 of the consent order.

full scale air sparging/soil vapor extraction system. O'Brien & Gere determined that the average PCE removal rate was equal to approximately 0.005 pounds per hour (page 9). They also found that in order to appropriately cover the proposed treatment area, a full scale system would have to consist of 80 injection wells and 9 extraction wells distributed across an area of approximately 200 feet by 40 feet (page 10). Page 10 of the Treatability Study indicates that the effective PCE removal rate for the ground water recovery system is approximately 0.02 pounds per hour. The primary conclusion of the Treatability Study presented on page 10, is that due to the large number of wells required for the full scale AS/SVE system and the relatively low expected PCE recovery rate, the design and installation of a full scale system is not recommended.

This paragraph essentially releases them from the requirements of Section VII. F of the Consent order

Based on U.S. EPA's evaluation of the information provided in the Treatability Study Report, U.S. EPA concurs with the conclusion that the design and installation of a full scale AS/SVE system for the Franklin site is not appropriate. Our primary rationale is that the very low PCE removal rate established during Treatability Study does not appear to warrant the costs associated with installing, operating and monitoring a full scale air sparging/soil vapor extraction system at the Franklin site.

The low PCE recovery rates may be the result of the relatively low concentrations of PCE in the groundwater at the site.

Thus, Franklin power products has in essence, fulfilled the requirements Webb Well Field Evaluation (May 5, 1999) of Section VII. F of the Consent

U.S. EPA reviewed the Franklin Power Products Webb Well Field Evaluation (May 5, 1999) prepared by O'Brien and Gere Engineers Inc. (O'Brien and Gere Evaluation). The primary purpose of the O'Brien and Gere Evaluation was to assess the report titled "Protecting Ground Water at the Indiana American Water Company's Webb Well Field Near Franklin, Indiana (June 30, 1997), by Wittman Hydro Planning Associates (WHPA Report) and to assess the validity of the primary conclusion of the WHPA Report that "DCE contamination at the Franklin Power Products facility is very likely ending up in the community drinking water supply" (Page 11).

The O'Brien and Gere Evaluation (pages 3 and 4) identifies deficiencies in the modeling and conclusions of the WHPA Report, and O'Brien and Gere (page 4) conclude that the modeling described in the WHPA Report cannot be used to demonstrate that the Franklin Power Products site is the source of volatile organic compounds (VOCs) detected in the Webb Well Field.

U.S. EPA does not disagree with the deficiencies identified by



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*Insert ①  
as a new paragraph.*

O'Brien and Gere in the WHPA Report and in fact, many of the deficiencies noted in the O'Brien and Gere Evaluation are similar to concerns that U.S. EPA identified during our 1998 evaluation of the WHPA Report. In addition, U.S. EPA agrees that the WHPA groundwater modeling described in the WHPA Report does not appear adequate to demonstrate that the Franklin Power Products site is the source of VOCs in the Webb Well Field. However, U.S. EPA also found that the O'Brien and Gere Evaluation did not provide any additional hydrogeologic information to refute this contention and to demonstrate that the Franklin Power Products site absolutely did not contribute to the VOC contamination detected at the Webb Well Field, and thus did not fulfill the requirements of Section VIII, I of the Consent Order.

One of U.S. EPA's recommendations from our 1998 evaluation of the WHPA Report was that Franklin should install additional temporary or permanent piezometers/monitoring wells in the area east and northeast of the Franklin site to 1) help demonstrate that the Webb Well Field pumping was not drawing groundwater from beneath the Franklin site, and 2) obtain additional information regarding the extent of the capture zone of the existing Franklin groundwater recovery and treatment system. Based on the statements made in the recommendations section of the O'Brien and Gere Evaluation (page 5), it does not appear that Franklin has, or intends to, install additional groundwater elevation monitoring points.

U.S. EPA notes that there is an additional factor that will complicate any evaluation of the source of VOCs in the Webb Well Field. The O'Brien and Gere Evaluation (page 3) indicates that the Webb Well Field was taken off-line in September 1997 and has only been used during times of drought conditions since that time. Since the Webb Well Field has not been pumping on a regular basis for almost two years, it is likely that the groundwater flow directions have returned to their original, non-pumping configuration. Therefore, it will not be possible to demonstrate whether or not the Franklin site contamination impacted the Webb Well Field without performing a long-term aquifer test using the Webb Well Field wells.

U.S. EPA does not believe that either party in this issue has provided adequate groundwater monitoring and groundwater modeling data to support any conclusion regarding whether the Franklin Power Products site is/was the source of VOCs detected in the Webb Well Field. U.S. EPA suggests that Amphenol and Franklin Power Products, Inc. not pursue this issue any further at this time unless, 1) Franklin or the Indiana American Water Company install and monitor additional groundwater level (and groundwater quality) monitoring points between the Franklin site and the Webb



Insert (1)

New Paragraph.

U.S. EPA recommends that Franklin install additional temporary or permanent piezometers/monitoring wells in the area east and northeast of the Franklin site to 1) help demonstrate that there is not ~~an~~ a natural, or web well field pumping induced, groundwater flow component towards the east or northeast, and 2) obtain additional information regarding the extent of the capture zone of the upgraded groundwater recovery and treatment system.



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~~Well Field, and 2) Franklin or Indiana American Water Company agree to perform a long-term aquifer test to determine the potential interaction between the Webb Well Field and the Franklin site. Please note that U.S. EPA is proposing that additional hydrogeological information is necessary for the Groundwater Recovery and Treatment System.~~ a/s

In summary, U.S. EPA has reviewed the Corrective Measures Implementation (CMI) Groundwater Recovery and Treatment System Upgrade Report; the Treatability Study Air Sparging/Soil Vapor Extraction (AS/SVE) System Report; and the Webb Field Evaluation Report that were submitted to U.S. EPA on May 6, 1999, by O'Brien & Geere Engineers, Inc. on behalf of Franklin Power Products, Inc. and Amphenol Corporation. Please provide responses to our comments and/or a revised version of the Corrective Measures Implementation Groundwater Recovery and Treatment System Upgrade Report within thirty (30) days from receipt of this letter. U.S. EPA suggested on page 2 of this letter that if the groundwater elevation adjacent to the storm sewer does not show a substantial continued decreasing trend during the first six months of operation, that Franklin implement other measures to prevent continued groundwater infiltration to the storm sewer. In addition, Section 2.5 Conclusions section of the Treatability Study: AS/SVE System report proposes further evaluation and possible enhancement of the upgraded on-site ground water recovery system as a feasible remedial alternative to the AS/SVE system. Please provide additional information on the possible enhancement of the on-site ground water recovery system. Also, U.S. EPA has identified some additional work on the Webb Well Field project. Please respond to our comments on the next steps for the Webb Well Field project/report with thirty (30) days from receipt of this letter.

If you should you have any questions please contact me at (312) 353-4921.

Sincerely,

Walt Francis, Project Manager  
Enforcement and Compliance Assurance Branch  
Waste, Pesticides and Toxics Division

Enclosure



6

cc: William Gabriel, O'Brien & Gere  
J. Michael Jarvis, Franklin Power Product (with enclosure)  
John Gunter, IDEM (with enclosure)

bcc: Larry Johnson, ORC (with enclosure)  
Dave Walker, TechLaw, Inc.



**FRANKLIN POWER PRODUCTS INC./AMPHENOL  
TECHNICAL REVIEW  
GROUND WATER RECOVERY AND TREATMENT SYSTEM  
UPGRADE REPORT**

**SPECIFIC COMMENTS**

1. Paragraph 2 on page 2 of the Ground Water Recovery and Treatment System Upgrade Report (Report) states, "To increase the individual yields of the existing three on-site recovery wells (RW-1, RW-2, and RW-3), existing pneumatic pumps and ancillary equipment were replaced with electric submersible pumps." However, the Report does not provide a description of the new equipment. The description should include but not be limited to the type and model number of the submersible pumps, the operating capacity of the pumps, and the depth at which the pumps were installed. This information is necessary in order to evaluate and understand how the recovery system was modified and the potential capability of the modified recovery system. ✓
2. Paragraph 5 on page 2 of the Report states, "Subsequent to completion, RW-4 was developed to remove fine grained sediments from the well screen and casing, and to promote hydraulic connection with the surrounding aquifer." However, the Report does not provide information regarding the well development methods used by the facility at RW-4. The Report should provide a full description of the methods used to develop RW-4, including the number of gallons removed during development, turbidity measurements collected during well development activities, and the amount of time required to develop the well. This information is necessary in order to evaluate well installation and development procedures and how it might impact the recovery system. In addition, if any aquifer tests were conducted at RW-4 to establish the optimum pumping rate for the well, those results should be presented in this Report. The Report should also include information regarding the type of pump installed in the new recovery well, the model of the pump, the pump's operating capacity, and the depth at which the pump was installed. ✓
3. Paragraph 7 on page 2 of the Report states, "Prior to installation of the electric pumps, the average flow from the recovery wells during January 8 to 29, 1999 was 9.1 gpm. Subsequent to installation of the electric pumps, the average flow as measured from March 10 to 25, 1999,



increased to 25.9 gpm." However, it is important to note that along with the replacement of the pneumatic pumps and ancillary equipment with electric submersible pumps, an additional recovery well (RW-4) was also installed at the facility to increase groundwater recovery operations. In order to understand better the differences in recovery rate using electric submersible pumps as opposed to pneumatic pumps, the Report should also present a calculated average pumping rate for each recovery well over an average 24-hour period. This information would better convey the realized increase in recovery rate based on replacing the pneumatic pumps with submersible electric pumps.

In addition, the Report states that the modified recovery system is operating 24 hours a day. However, the Report does not provide any information on the system's method of operation. The Report should include a description of how the modified system is operated. For instance, are the pumps within the recovery wells operated on a continuous basis or are the pumps cycled using timers or float switches.

4. Paragraph 1 on page 3 of the Report states, "The figure (Figure 2) shows that under static conditions, ground water flows from north to south across the site." However, the Report does not provide sufficient data to support this statement. Based on Figure 2 it appears that the pre-upgrade groundwater elevation contour map was prepared using static groundwater levels collected at only 10 of the 19 available water level monitoring points shown on the map. No static water levels were collected between monitoring wells MW-9 and MW-21, and it does not appear that there are any water level monitoring points located along the far eastern and western boundaries of the site. The only area of the site where sufficient data were gathered to verify static groundwater flow was from the southeastern portion of the site and even there, data was not collected from MW-23, MW-25, IT-2 and IT-3. Therefore, the statement that Figure 2 shows that groundwater flows from "north to south across the site" is not fully supported by the data presented in this Report. To support the interpreted groundwater flow direction for the site, additional groundwater elevation monitoring points could be installed along the eastern property line between MW-9 and MW-30 and along the western property line.
- walt, these suggested wells will help show if there is a NE component of GW flow toward Webb Field*



5. Paragraph 1 on page 3 of the Report indicates that Figure 3 depicts ground water flow conditions during active pumping of the upgraded system. Figure 3 shows that well developed cones-of-influence have been developed by the recovery wells, which extend across the site to the downgradient property boundary. However, the Report does not provide sufficient data to support this statement.

The groundwater contour elevations depicted in Figure 3 represent the facility's interpretation of the groundwater elevation data collected during the operation of the upgraded recovery system. However, based on the groundwater elevation data presented in Figure 3, it is not clear whether the cones-of-influence actually extend across the site between RW-4 and RW-3. Note that U.S. EPA is aware that it may be difficult to obtain data to conclusively demonstrate that the cones of influence between the two pumping wells actually intersect due to problems associated with installing piezometers on the residential property south of RW-4. However, the installation of even a temporary piezometer on the residential property west of MW-22 would provide much needed data.

In addition, it does not appear that the interpreted cone-of-influence from RW-4 extends to the western property boundary of the facility. Therefore, the statement that the cones-of-influence extend across the site to the downgradient property boundary is not supported by the data presented in this Report for the portion of the facility west of RW-3.

To support and verify the interpretations of static groundwater flow present at the site and cones-of-influence that result from the operation of the groundwater recovery system, the facility should install additional monitoring points in the form of piezometers or additional groundwater monitoring wells west and south of RW-4.

6. The second bullet under the conclusions section on page 3 of the Report states, "The cones-of-influence developed by the ground water recovery wells extend across the site to the downgradient property boundary providing a hydraulic barrier to off-site groundwater flow." This statement implies that the recovery wells are providing containment of groundwater flow across the site and that this containment prevents groundwater from flowing off-site. Data which demonstrates capture zones for each of the recovery wells have not been

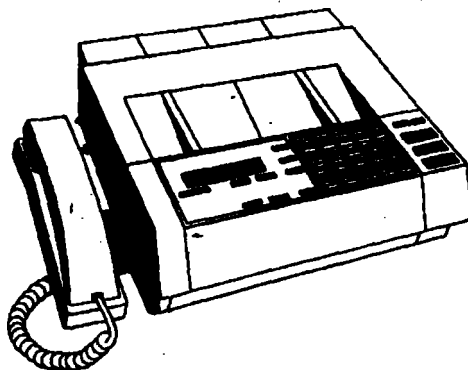


provided in this Report since based on Figure 3, it does not appear that there are an adequate number of groundwater elevation monitoring points along the southeastern and southern property boundaries to verify the size of the capture zones in the area south, east and west of RW-1 and RW-2.

To support and verify the modified groundwater recovery system's ability to contain the on-site groundwater, Franklin should install additional groundwater elevation monitoring points at intervals along Hamilton Avenue from the intersection with Upper Shelbyville Road to a point where an extension of the western property boundary would intersect Hamilton Avenue. In addition, the facility should conduct groundwater modeling using data from on-site monitoring and recovery wells and all newly installed groundwater elevation monitoring points to support that containment is achieved through the operation of the current on-site recovery system. The modeling should include particle transport modeling to verify capture. Note that if site specific data has not already been obtained, additional aquifer testing may be required to derive parameters such as hydraulic conductivity, transmissivity, and storativity.

**Waste Pesticides & Toxics Division  
Enforcement & Compliance Assurance Branch  
U.S. Environmental Protection Agency  
Region 5  
77 West Jackson Boulevard  
Mailcode: DRE-9J  
Chicago, Illinois 60604**

**FACSIMILE REQUEST**



To: DAVE WALKER  
Office/Phone: (303) 763-7188  
Facsimile Number: (303) 8763-4896  
Verification Number: —

From: WALT FRANKS  
Office/Phone: (312) 353-4821  
Date: 9/16/99 Number of Pages: 11  
Additional Comments:

**FACSIMILE NUMBER:  
312/353-4342**